the sample in V_U is

$$\beta = -\frac{1}{V_U} \frac{dV_U}{dP_U} = \frac{S_L}{V_U} \left(\frac{dP_L}{dP_U} - \frac{S_U + S_L}{S_L} \right). \tag{1}$$

Generally, the values of ΔP are small enough to represent the differentials directly. With the cell characteristics V_{U_0} =0.3380 cm³, S_U =1.31×10⁻³ cm³ atm⁻¹, and S_L =1.09×10⁻³ cm³ atm⁻¹,

$$\beta \approx 2.5 \times 10^{-3} (\Delta P_L / \Delta P_U - 2.2) \text{ atm}^{-1}$$
. (2)

B. Apparatus

The *P-V-T* cell was made from Be-Cu (Berylco-25) disks, welded together by an electron beam, then heattreated for favorable strength and elasticity. The cell was designed to measure a range of $\Delta V/V$ values from 5×10⁻⁵ for thermal expansion to 10⁻¹ for melting, a much greater range than needed here for the liquid compressibility. At 4°K, the diaphragm displacement at the center was 3×10-4 cm atm-1 up to the maximum working pressure of 68 atm. The upper diaphragm deflection was measured with a Sanborn 959 DT 005 differential transformer, whose output was put through a Sanborn 311 amplifier and read on a Weston dc voltmeter. The resolution of 0.01 V corresponded to 10-3 atm. The sensitivity was frequently checked between compressibility measurements against a room-temperature gauge. The diaphragm behavior seemed to stay constant, but the over-all sensitivity varied slightly with bath height (an effect of lead resistance) and with axial position of the transformer core.

The volume of the upper (sample) chamber was calibrated against various pressures in the upper and lower chambers by metering withdrawn helium, gas at 296 and 76°K, liquid at 4°K. The molar volumes at 4°K were taken from Edeskuty and Sherman⁵ after a -0.30% correction. The observed values of the volume sensitivity increased with temperature, 5% for 4 to 76°K and 14% for 4 to 296°K but were constant with pressure to 68 atm.

A rigid requirement in the ΔV measurements was the tightness of the valve sealing the sample in the cell. The valve tip was a 55° cone of Teflon; its seat was a 0.5-mm hole in the brass body. A leak test after each closing showed the valve to be tight in all cases.

The pressure standards were: (a) a Consolidated Electrodynamics Corp. 6-201 gas piston gauge to 34 atm; and (b) an Ashcroft 1313A oil piston gauge to 68 atm. The first was calibrated against other standard gauges and the CO₂ sublimation pressure at the ice point; accuracy was better than 0.01%. Both piston gauges had calibrated weights so that pressure changes

Fig. 2. Isothermal compressibility coefficient versus pressure for liquid He⁴ at several temperatures. The measurements show no deviation from the curves on this scale.

of 0.3 atm were known to 0.01%; this was useful in checking the consistency of the *P-V-T* cell diaphragm sensitivity. Routine pressure measurements were made with Heise and Seegers Bourdon-type and Consolidated diaphragm-type gauges.

Temperatures of the liquid He⁴ bath were determined from vapor pressures on the "1958 Scale".⁶ The bath pressure was regulated to less than 0.5 mdeg equivalent.

III. RESULTS

The isothermal compressibility coefficient β was measured directly over a wide pressure range, usually from about 1 atm to the melting pressure, for temperatures between 1.60 and 2.50°K. Typical results are shown in Fig. 2. The 2.20°K curve illustrates the monotonic decrease of β with increasing pressure for

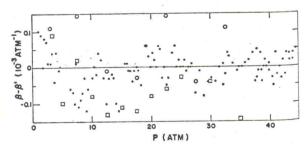


Fig. 3. Deviations of liquid He⁴ compressibility at 2.200°K from $0.30 \times 10^{-3} + (72.0 \times 6.66P)^{-1}$. • present measurements of derived from density data of Keesom and Keesom (Ref. 1): derived from density of Edeskuty and Sherman (Ref. 5).

<sup>2.05°
2.05°
2.05°
10
2.00°
1,55°
1,75°
1,74°
1,70°
1,65°
2,20°
2,20°</sup>

⁵ F. J. Edeskuty and R. H. Sherman, in Low Temperature Physics and Chemistry, edited by J. R. Dillinger (University of Wisconsin Press, Madison, Wisconsin, 1958), p. 102.

⁶ F. G. Brickwedde, H. van Dijk, M. Durieux, J. R. Clement and J. K. Logan, J. Res. Natl. Bur. Std. (U. S.) 64A, No. 1 (1960)